

**REMARKS**

Claims 1-18 and Claim 27 are active in the case.

The present invention relates to a process for the upgrading of hydrocarbon mixtures that boil within the naphtha range and which contain sulfur impurities.

**Specification Amendments**

The specification has been amended at pages 9 and 13 to correct the spelling of heptamolibdate to heptamolybdate and to correct several formulas. None of the amendments introduce new matter into the case. Entry of the amendments is respectfully requested.

**Claim Amendments**

Claim 1 has been amended in order to place the format of the process claim in more conventional U.S. claim format. No substantive language changes have been made to the claim. Further, Claims 2 to 18 have been amended to improve upon the syntax of the claims and in order to correct spelling errors. Claims 17 and 18 have been amended in order to convert the language of these claims to the singular form. None of the amendments made introduce new matter into the record.

Claim 27 has been added in order to more closely define the hydrocarbon mixture being treated by the present process in terms of a naphtha as described in the last paragraph on page 5 of the text. Entry of the claim into the record is respectfully requested.

Prior Art Rejection

As claimed, the present invention is a process of hydrodesulfurizing a hydrocarbon mixture, by reacting a hydrocarbon mixture containing olefins and having a boiling range within the range of C<sub>4</sub> to 250° C, and a sulfur content of at least 150 ppm with hydrogen in the presence of a catalytic composition comprising:

a) an acidic carrier consisting of a silica and alumina gel, amorphous to X-rays, with a molar ratio SiO<sub>2</sub>/Al<sub>2</sub>O<sub>3</sub> of 30/1 to 500/1, having a surface area ranging from 500 to 1000 m<sup>2</sup>/g, a porosity of 0.3 to 0.6 ml/g and a pore diameter within the range of 10-40 Å;

b) a mixture of metals belonging to Groups VIB and VIII of the Periodic Table deposited on the carrier in an overall quantity ranging from 2 to 67 % by weight with respect to the total amount of components (a) + (b), thereby effecting said hydrodesulfurization with concomitant skeletal isomerization of the olefins of said mixture.

Applicants emphasize that the hydrocarbon mixture is one which boils within the stated range and is a mixture of both paraffinic hydrocarbons and olefins. In fact, a preferred embodiment of the hydrocarbon mixture is a full range naphtha having a boiling range of 35° -250° C. As a result of contacting the hydrocarbon mixture with hydrogen in the presence of the catalyst as defined in the claims, not only is significant hydrodesulfurization of the mixture obtained, but also importantly, from the viewpoint of obtaining a hydrocarbon product that exhibits a high octane rating, the olefin component of the hydrocarbon undergoes significant isomerization with minimal hydrogenation of the olefins to paraffinic material.

Claims 1-18 stand rejected based on 35 USC 103(a) as obvious over Hart U.S. Patent 3,156,640 in view of Bellussi et al EP-340868. This ground of rejection is respectfully traversed.

Although the Hart patent discloses a process of hydrogenating a hydrocarbon material that contains olefins over a metal containing supported catalyst that achieves hydrodesulfurization, the hydrocarbon material of the patent is **not** that which is employed in the present process and further the metal containing catalyst is not that of the present invention.

As to the hydrocarbon material employed in the patent, the same is a combination of an olefin rich hydrocarbon mixture (see Example 1, col 5, lines 53-59) and a sulfur-containing hydrocarbon oil fraction that is said to have a low content of olefinic components (col 2, lines 40-42). (The sulfur containing hydrocarbon component functions as a diluent for the olefin containing paraffin in order to reduce the undesirable effects of excessive exothermicity of the hydroisomerization of the olefin component to isoparaffin materials.) The objective of the catalyzed hydrogenation reaction is not only reduction in the sulfur content of the product obtained, but also the isomerization of the olefins in the hydrocarbon mixture to isomeric structures while at the same time **achieving reduction of the isomeric structures to saturated isoparaffins**. (See column 1, lines 46-51. Note also as shown in Example 1 that extensive hydrogenation of olefins occurs as the olefin content (62 %) of the starting hydrocarbon mixture is reduced to the extent that the hydrocarbon product obtained is "practically free of olefins" (bromine number of < 1.) On the other hand, the hydrocarbon

feed of the present process is not such a combination, but rather is a hydrocarbon mixture that boils within the stated range which contains from low to higher olefin contents. (A "full range naphtha" boiling over the range of 35° to 250° C is a particularly preferred hydrocarbon mixture employed in the process of the invention.) In the catalyzed reactions that occur, the olefins within the mixture are extensively isomerized to **unsaturated** isomers, however, with **minimal** reduction of the isomerized unsaturated isomers obtained to saturated isomers. The reason for the sought after minimal reduction of olefinic material is that the presence of unsaturates in the hydrocarbon product yields a product of higher octane rating or number. Thus, the product desired and achieved by the present process which contains isomerized olefinic material that has experienced minimal reduction to saturated isomers is distinctly different from the reaction product of Hart that is "practically free from olefins."

The objective of the present process of olefin isomerization with minimal reduction during the hydrodesulfurization reactions which occur is shown, for instance, by the catalyst embodiment of the invention of Example 8 in Table 2 on page 20 of the text. Note that at the temperatures indicated, extensive hydrodesulfurization occurs as shown in the column "HDS%," significant amounts of isomerized unsaturated hydrocarbon remains as shown in the column "ISO%" relative to reduced hydrocarbon ("HYD%") and the ratio of HYD/ISO is 1 or slightly greater. On the other hand, for a comparative catalyst system as that of Catalyst F (Example 11), the columns ISO%, HYD% and HYD/ISO show a low content of isomerized unsaturates accompanied by extensive reduction of olefinic material to saturated

hydrocarbons. Catalyst F, in fact, is a commercial catalyst of Co and Mo impregnated in a support of  $\gamma$ -alumina which is a type of catalyst within the scope of Hart.

A second important distinction of the invention as claimed over the Hart patent is that the present specific high silica content catalyst support is markedly different from the acid carriers described in column 4 of the patent which are stated broadly as silica, alumina and silica-alumina supports. There is absolutely no teaching or suggestion of the specific support of the present claims which has the specific characterizations set forth in Claim 1. Yet, it is the support of the catalyst system of the present process which enables the very desirable results obtained in the present invention for the production of a hydrocarbon product having a relatively high unsaturated isomer content with minimal reduction of unsaturates to saturated hydrocarbon.

The deficiencies of Hart are believed to be neither overcome or improved upon by Bellussi et al. It is clear that the silica/alumina material disclosed of Bellussi et al is the same material which is used as the support for the catalytically active Group VIII and VIB metals used to prepare the catalyst system of the present invention which achieves the hydrodesulfurization results of the present invention. The Examiner notes the disclosure in the publication that the catalyst system disclosed in the reference, which is the silica/alumina material described with no added metal, is useful in the catalysis of olefin isomerization reactions. However, the unsaturated feedstock employed by Bellussi et al selectively is an olefinic feedstock which is **not** the hydrocarbon mixture employed in the present process. Example 10 of the reference provides three specific examples of olefin feedstocks which are

(1) 1-octene, (2) a mixture of linear isomers of tetradecene and (3) 7-tetradecene. The isomerization reaction does **not** occur in the presence of hydrogen. Moreover, whereas in the present process a significant degree of selectivity of olefin isomerization to isomeric unsaturated products is achieved while at the same time competing hydrogenation reactions that convert unsaturated material to isoparaffins and accomplish hydrogenative desulfurization of the feed to the reaction occur, no such competition occurs in the olefin isomerization reaction taught in Bellussi et al. Because the comparatively simple olefin isomerization process taught in the reference is fundamentally different from the hydrodesulfurization reaction of the present invention which occurs in the presence of a metal containing catalyst supported on the specific support described, one of skill in the art would not be led to attempt to preferentially use the silica/alumina isomerization catalyst taught by Bellussi et al as a support for a catalytically active metal for use in a hydrodesulfurization reaction over any other silica, alumina or silica/alumina support known in the art.

Applicants again stress with respect to the disclosure of Bellussi et al that the reactions catalyzed by silica-alumina gel in the reference, as disclosed in the first paragraph on page 4 are (1) dimerization of olefins (particularly linear olefins), (2) isomerization of butenes, (3) alkylation of hydrocarbons with olefins and (4) dewaxing. The isomerization reactions disclosed do **not** require hydrogen as a reactant, and accordingly, the activity of the catalyst employed is solely in the context of the isomerization of olefinic hydrocarbons. There is no teaching or suggestion of the behavior of the catalyst when both olefins and

hydrogen are present in the same reaction mixture. This is very significant because one of skill in the art would expect that with the acidic catalyst of Bellussi et al, in the presence of hydrogen, **extensive hydrogenation** of olefins would occur. The finding of the present invention, to the contrary, is that with the use of the catalytic composition of the present invention, it is possible to **desulfurize** a mixture of hydrocarbons that contains olefins and sulfur, and at the same time achieve skeletal isomerization of the olefin component of the hydrocarbon mixture with a concomitant **low degree of hydrogenation** of olefinic double bonds.

In support of the comments immediately above, applicants refer to the data of the catalytic compositions of Hart, the data in Table 7 on page 24 of the present specification which show the lower hydrogenation/isomerization (HYD/ISO) ratios of catalyst embodiments (B, C, E) of the present invention versus comparative catalysts F and G outside the scope of the invention, particularly catalyst G, as well as the data indicated in the table below of a comparative catalyst similar to, but outside the scope of the present catalyst. (The data of the table is found in the accompanying declaration.) The comparison between the catalyst of the present invention (B,C,E) and comparative catalysts F and G, as well as the data indicated in the table below of a comparative catalyst similar to, but outside the scope of the present catalyst, shows also higher hydrodesulfurization/hydrogenation (HDS/HYD) ratios for catalysts B, C and E.

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Temp (°C)	WHSV (hrs <sup>-1</sup> )	HDS (%)	ISO (%)	HDS/HYD	HYD/ISO
254	6.6	91.0	2.5	1.2	29.9
282	6.6	92.7	2.5	0.9	40.4

Accordingly, the combined prior art references do not suggest the invention as claimed and withdrawal of the rejection is respectfully requested.

It is now believed that the application is in proper condition for allowance. Early notice to this effect is earnestly solicited.

Respectfully submitted,

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